

Productividad Académica de la LGAC de Biotecnología Microbiana

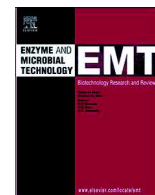
Las publicaciones de los PTC de la LGAC de Biotecnología Microbiana, en comparación con el periodo anterior, se incrementaron en este periodo de evaluación y se publicaron en revistas de mejor impacto, mientras se han enfocado en tres temáticas básicas: *i)* fermentación alcohólica de agave y aprovechamiento de las levaduras asociadas, *ii)* valorización de subproductos e insumos de bajo valor comercial y, *iii)* biorremediación de suelos. Así mismo, se ha colaborado con grupos de investigación de otras instituciones, en investigaciones relacionadas con las temáticas ya mencionadas.

La labor científica de la LGAC se complementa con la colaboración con grupos de investigación de otras instituciones, tanto nacionales como extranjeras, en donde se han generado un total de 13 artículos de investigación en colaboración con estudiantes en el periodo, de los cuales 12, son con estudiantes de doctorado

PRODUCCIÓN ASOCIADA A LOS ESTUDIANTES-PTC MIEMBROS DE LA LGAC BIOTECNOLOGIA MICROBIANA.

BIOTECNOLOGIA MICROBIANA	
1	Vazquez-Ortega, P. G., Alcaraz-Fructuoso, M. T., Rojas-Contreras, J. A., López-Miranda, J., & Fernandez-Lafuente, R. (2018). Stabilization of dimeric β -glucosidase from <i>Aspergillus niger</i> via glutaraldehyde immobilization under different conditions. <i>Enzyme and microbial technology</i> 110, 38-45.
2	Sánchez-Castañeda, A. K., Athès, V., Moussa, M., López-Miranda, J., Páez-Lerma, J. B., Soto-Cruz, N. Ó., & Trelea, I. C. (2018). Modeling of isoamyl acetate production by fermentation with <i>Pichia fermentans</i> in an aerated system coupled to in situ extraction. <i>Process Biochemistry</i> .65, 11-20
3	Bailón-Salas, A. M., Ordaz-Díaz, L. A., Valle-Cervantes, S., Lopez-Miranda, J., Urtiz-Estrada, N., Páez-Lerma, J. B., ... & Rojas-Contreras, J. A. (2017). Bacterial Diversity in Two Aerated Lagoons of a Pulp and Paper Effluent and their Interaction with a Commercial Inoculum using PCR-DGGE. <i>BioResources</i> , 12(3), 5487-5501.
4	Cisneros de la Cueva S., Hernández Rodríguez C., Soto Cruz, N.O., Rojas-Contreras, J.A., López-Miranda, J. (2016) Changes in Bacterial Populations During Bioremediation of Soil Contaminated with Petroleum Hydrocarbons Water, Air, & Soil Pollution, Vol.227, Pag.1-12.
5	Cisneros-de la Cueva, S., Martínez-Prado M.A., López-Miranda, J., Rojas-Contreras, J.A. and H. Medrano-Roldán H. (2016) Aerobic degradation of diesel by a pure culture of <i>Aspergillus terreus</i> kp862582 , Revista Mexicana de Ingeniería Química, Vol.15, Pag.347-360.
6	Nuñez-Guerrero M.E., Páez-Lerma J.B., Rutiaga-Quiñones O.M., González-Herrera S.M., Soto-Cruz O.N. (2016). Performance of mixtures of <i>Saccharomyces</i> and non-<i>Saccharomyces</i> native yeasts during alcoholic fermentation of <i>Agave duranguensis</i> juice . <i>Food Microbiology</i> . 54, 91-97.
7	De los Rios-Deras, G.C., Rutiaga-Quiñones, O.M., López-Miranda, J., Páez Lerma, J., López, M.G. and Soto-Cruz, N.O (2015). Improving <i>Agave duranguensis</i> must for enhanced fermentation , Revista Mexicana de Ingeniería Química, Vol.14, Pag.363-371.
8	Alma D. Orozco-Cortés, Gerardo Álvarez-Manilla, Gerardo Gutierrez-Sánchez, Olga M. RutiagaQuiñones, Javier López-Miranda and Nicolás O. Soto-Cruz. (2015) Characterization of fructans from <i>Agave duranguensis</i> . <i>African Journal of plant Science</i> . 9(9), pp. 360-367
9	Rodríguez-Sifuentes, L., Páez-Lerma, J.B., Rutiaga-Quiñones, O.M., Ruíz-Baca, E., Rojas-Contreras, J.A., Gutiérrez-Sánchez, G., Barrio, E. and Soto-Cruz, N.O. (2014). Identification of a yeast strain as a potential stuck wine fermentation restarter: a kinetic characterization . <i>CyTA Journal of Food</i> ., Vol.12, Pag.1-8.
10	Ordaz-Díaz L.A., Rojas-Contreras J.A., Rutiaga-Quiñones O.M., Moreno-Jiménez M.R., Alatríste-Mondragón F. and Valle-Cervantes S. (2014). Microorganism degradation efficiency in bod analysis formulating a specific microbial consortium in a pulp and paper mill effluent . <i>Bioresources</i> . 9. 7189-7197.
11	Hernández-Carbajal, G.R., Rutiaga-Quiñones, O.M., Pérez-Silva, A, Saucedo-Castañeda, G., Medeiros, A.B.P., Soccol, C.R, and Soto-Cruz, N.O. (2013). Screening of native yeast from <i>Agave duranguensis</i> spontaneous alcoholic fermentation with potential for production of Isoamyl acetate . (<i>Brazilian Archives of Biology and Technology</i> . Vol.56, Pag.357-363.
12	Páez-Lerma, J. B. Arias-García, A., Rutiaga-Quiñones, O. M., Barrio, E. and Soto-Cruz, N. O. (2013). Yeasts isolated from the alcoholic fermentation of <i>Agave duranguensis</i> during mezcal production , <i>Food Biotechnology</i> , Vol.27. 342-356.
13	Fileto-Pérez H.A., Rutiaga-Quiñones J.G., Aguilar-González C.N., Páez J.B., López J. and Rutiaga-Quiñones O.M. (2013). Evaluation of <i>Eichhornia crassipes</i> as an Alternative Raw Material for Reducing Sugars Production . <i>Bioresources</i> .8 (4) 5340-5348.

<p>cuatro variedades (pinto villa, pinto saltillo, pinto mestizo y flor de mayo). Revista Mexicana de Ingeniería Química, Vol.10, Pag.17-28.</p>



Stabilization of dimeric β -glucosidase from *Aspergillus niger* via glutaraldehyde immobilization under different conditions

Perla Guadalupe Vazquez-Ortega^{a,b,1}, Maria Teresa Alcaraz-Fructuoso^{a,1},
Juan A. Rojas-Contreras^b, Javier López-Miranda^{b,*}, Roberto Fernandez-Lafuente^{a,**}

^a Departamento de Biocatálisis, ICP-CSIC, Campus UAM-CSIC Cantoblanco, Madrid, Spain

^b TECNOLÓGICO NACIONAL DE MÉXICO, INSTITUTO TECNOLÓGICO DEDURANGO, Blvd. Felipe Pescador 1130 Ote. Col., Nueva Vizcaya, CP 34080, Durango, Dgo., México



ARTICLE INFO

Keywords:

Stabilization of multimeric enzymes
Glutaraldehyde versatility
Enzyme immobilization
Improved enzyme activity upon immobilization
Amino-agarose beads
Glucosidase

ABSTRACT

The dimeric enzyme β -glucosidase from *Aspergillus niger* has been immobilized on different amino-agarose beads at pH 5 and 7, exploiting the versatility of glutaraldehyde. The stability of the free enzyme depended on enzyme concentration. Immobilization via ion exchange improved enzyme stability/activity, depending on the immobilization pH. However, the enzyme was desorbed in 75 mM NaCl at pH 7 and some stability/enzyme concentration dependence still existed.

Treatment: of these biocatalysts with glutaraldehyde increased enzyme stability (e.g. at pH 5, after incubation under conditions where the enzyme just ionically exchanged was fully inactivated, the activity of the glutaraldehyde treated enzyme remained unaltered). Immobilization on glutaraldehyde pre-activated supports yielded a higher increase in enzyme activity, but the stabilization was lower. While when measuring the enzyme activity at pH 4 there were no changes after immobilization, all immobilized enzymes were more active than the free enzyme at pH 6 and 7 (2–3 times). The K_i/K_m ratio did not significantly decrease in any immobilized biocatalysts, and in some cases it worsened in a significant way (by a 9 fold factor using preactivated supports). The new biocatalysts are significantly more stable and avoid enzyme subunit desorption, being the immobilization pH a key point in their design.

1. Introduction

The demand for renewable energy sources has moved from biodiesel to bioethanol produced from lignocellulosic materials, the most abundant polymers in nature [1–4]. Lignocellulosic biomass is one of most promising renewable feedstocks for ethanol production, which is a suitable fuel, due to its high octane number, vaporization heat, and compatibility with motor vehicles [5]. The first step in the production of bioethanol is the hydrolysis of cellulose to get glucose. In this regard, the use of enzymes presents some advantages, like the prevention of side-reactions produced using acid catalysis that can hinder the fermentation process [1–4,6].

The enzymatic hydrolysis of cellulose is accomplished from the synergistic action of endoglucanases, exoglucanases I and II and β -glucosidases. These enzymes are found commonly in fungal species (*Penicillium verruculosum*, *Trichoderma reesei*, *Aspergillus niger*, *Sporotrichum thermophile*) [7]. The first enzymatic hydrolytic steps are

performed by endoglucanase and exoglucanase activities, and they produce elevated concentrations of cellobiose (a reducing sugar that is formed by two β glucose molecules linked by a β (1 \rightarrow 4) bond), which is the substrate of β -glucosidase [8,9]. β -glucosidases may be applied in other processes such as fine chemicals and medicines production [10]. Thus, they are also used to produce the release of some glycosylated substances (like flavors or terpenes in wine and other products [11–18]) or the production of some glycosylic bonds [19–21]. The importance of β -glucosidases in industrial and environmental processes has been summarized in different reviews and investigations [22–24].

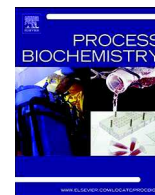
Thus, biocatalysis is a good option to transform cellulose into glucose, but some problems, such as the price and moderate enzyme stability under operational conditions are hindering their industrial implementation [25,26]. One solution to both problems may be enzyme immobilization. If the immobilized enzyme is stable enough, it may be reused, and that will decrease the final price of the biocatalyst [27–30]. A proper immobilization may improve enzyme stability via multipoint

* Corresponding author.

** Corresponding author at: Corresponding autor: ICP-CSIC,C/Marie Curie 2, Campus UAM-CSIC, Cantoblanco, 28049 Madrid, Spain.

E-mail addresses: jlopezym@gmail.com (J. López-Miranda), rfl@icp.csic.es (R. Fernandez-Lafuente).

¹ Both authors have evenly contributed to this paper.



Modeling of isoamyl acetate production by fermentation with *Pichia fermentans* in an aerated system coupled to *in situ* extraction



Ana Karen Sánchez-Castañeda^{a,b}, Violaine Athès^a, Marwen Moussa^a, Javier López-Miranda^b, Jesús Bernardo Pérez-Lerma^b, Nicolás Óscar Soto-Cruz^b, Ioan Cristian Trelea^{a,*}

^a UMR 782 Génie et Microbiologie des Procédés Alimentaires (GMPA), AgroParisTech, INRA, Université Paris-Saclay, F-78850 Thiverval-Grignon, France

^b Tecnológico Nacional de México, Instituto Tecnológico de Durango, Departamento de Ingenierías Química-Bioquímicas, Blvd. Felipe Pescador 1830 Ote, Col Nueva Vizcaya, Durango, Dgo 34080, Mexico

ARTICLE INFO

Chemical compounds studied in this article:

Isoamyl acetate (PubChem CID: 31276)

Decane (PubChem CID: 15600)

L-leucine (PubChem CID: 6106)

Keywords:

Aroma production

Fermentation kinetics

Partition coefficient

Simulation

Natural flavoring substance

ABSTRACT

This study deals with the production of isoamyl acetate (IAA) by fermentation of sugar cane molasses with the strain *Pichia fermentans* ITD00165, using L-leucine as precursor. A mathematical model that describes the experimental data from fermentation was developed for its use as a tool for further process optimization. The fermentation system was constantly aerated and coupled to liquid–liquid *in situ* extraction with decane as the recovery solvent. Thus, the model integrates the biological production of IAA, its partition coefficient in the two liquid phase system and the stripping effect of aeration. A productivity of $26 \text{ mg L}^{-1} \text{ h}^{-1}$ was obtained with addition of 4 g L^{-1} of L-leucine at 12 h of fermentation. The use of the model for process optimization was explored. According to it, the maximum theoretical productivity that can be obtained is $63 \text{ mg L}^{-1} \text{ h}^{-1}$. The model was used to determine that 1.6 g L^{-1} is the minimum concentration of L-leucine that can be added without significantly reducing IAA production. Also, it makes possible to propose an adequate decane/culture medium ratio, to have a desired final concentration and amount of recovered IAA. This value can be adjusted based on the needs of further purification steps and is useful to define a global economic optimum of the process.

1. Introduction

Esters of short-chain fatty acids are important flavor and fragrance compounds widely used in the food and beverage industries. Isoamyl acetate (IAA) is characterized by its strong smell of banana which gives it a very important place in food, pharmaceutical and perfumery industries with a demand of 75 tons per year in USA alone in 2010 [1–3], increasing over the years. This substance is obtained by chemical synthesis, extraction from natural sources, or fermentation [4].

In recent years, the interest towards the production of flavor compounds through white biotechnology processes over traditional methods has increased. Principal reasons are that chemical synthesis often consists in an environmentally unfriendly production process, with important drawbacks such as poor reactions selectivity resulting in racemic mixtures, low yields, and high downstream costs [5,6]. Also, consumers have developed an apprehensive attitude towards these synthetic compounds, especially if the products are related to food or domestic usage. Moreover, the extraction of flavoring compounds from natural sources gives very low yields and has potential difficulties with

obtaining the raw material [3,4,7]. Contrary to chemical synthesis, flavors obtained by fermentation can have the “natural flavoring substance” classification by the European (EC No 1334/2008) and U.S. (21CFR101.22) regulations, which allows using them safely as an additive in food and beverages. This has been the main reason for developing biochemical processes over the years, but presently, after years of research, the inherent advantages of white biotechnology processes are the driving force for its application: operation under mild and more environmentally friendly conditions, as well as chemical and stereo specificity of the obtained compounds, are the most important ones [8].

There are several published studies focused on IAA biological production. They include enzymatic synthesis using lipases and esterases [1,3,9–15] and fermentation process by microorganisms, especially yeasts strains [6,16–20]. Whole cell fermentation can be a more economical method than enzymatic systems and easier to scale up to industrial level. There are some encouraging studies with interesting IAA productivities in the literature; for example, Yilmaztekin et al. [6] used a *Williopsis saturnus* strain in a medium composed of beet molasses and

* Corresponding author.

E-mail addresses: ana-karen.sanchez@inra.fr (A.K. Sánchez-Castañeda), violaine.athes-dutour@inra.fr (V. Athès), marwen.moussa@agroparistech.fr (M. Moussa), jlopez@itdurango.edu.mx (J. López-Miranda), jpaez@itdurango.edu.mx (J.B. Pérez-Lerma), nsoto@itdurango.edu.mx (N.Ó. Soto-Cruz), cristian.trelea@agroparistech.fr (I.C. Trelea).

<http://dx.doi.org/10.1016/j.procbio.2017.10.010>

Received 8 June 2017; Received in revised form 12 October 2017; Accepted 15 October 2017

Available online 16 October 2017

1359-5113/ © 2017 Elsevier Ltd. All rights reserved.

Bacterial Diversity in Two Aerated Lagoons of a Pulp and Paper Effluent and their Interaction with a Commercial Inoculum using PCR-DGGE

Ana M. Bailón-Salas,^{a,δ} Luis A. Ordaz-Díaz,^b Sergio Valle-Cervantes,^a Javier López-Miranda,^a Norma Urtiz-Estrada,^c Jesús B. Páez-Lerma,^a Gerardo D. de León-Mata^b and Juan A. Rojas-Contreras^{a,*}

Aerated lagoons are a main unit operation for wastewater treatment in the paper industry. Many such operations involve inoculation with bacterial formulations in which *in situ* effectiveness has not been proven; this can be translated into low efficiency in treatment and unnecessary investments. Lack of knowledge of bacterial biodiversity present in a lagoon limits the capacity to exploit the maximum degradation. To overcome such problems, various methods to identify and study these microorganisms have been developed. In this study, a PCR-DGGE analysis was performed to estimate the bacterial diversity and to verify the presence of bacteria present in a commercial inoculum in two aerated lagoons of a pulp and paper effluent. Phylogenetic affiliation of predominant member's correspondent to γ - and β -proteobacteria and Firmicutes were found. The dominant bacteria present in lagoon 2 belonged to the following genus *Microbacterium* sp. *Rhodocyclaceae* sp., *Eubacterium* sp. and *B. subtilis*. In lagoon 1 the dominant genus included *Microbacterium* sp., *Rhodocyclaceae* sp. *Tepidimonas* sp., *Acetanaerobacterium* sp., and *Flavobacteria* sp. The two characterized lagoons were not similar to the commercial inoculum. In addition, non-dominant bacteria (less relative intensity) were composed mostly of bacteria of the commercial inoculum.

Keywords: Pulp and paper effluent; Bacterial diversity; PCR-DGGE; 16S rDNA; Commercial inoculum

Contact information: a: Chemical and Biochemical Engineering Department, Durango Institute of Technology (ITD), Durango, México; b: Environmental Engineering Technology, Universidad Politécnica de Durango, Durango, México; c: Facultad de Ciencias Químicas, Universidad Juárez del Estado de Durango, Durango, México; ^δPhD Student; *Corresponding author: juanroco@hotmail.com

INTRODUCTION

Wastewaters of pulp-and-paper mills can be potentially polluting and very dangerous, so they should be treated before being discharged (Ashrafi *et al.* 2015). The most common aerobic biological methods used in the treatment of pulp mill effluents are aerated lagoons (Bajpai 2012). Of the microorganisms involved in the depuration process, bacteria stand out; they are able to convert organic matter to carbon dioxide, water, and biomass, which can be removed by physical methods (Welander *et al.* 1997; Forster *et al.* 2003). The stability and permanence of bacteria in the system ensures an efficient process. However, lagoons are subjected to various perturbations such as variations in pH, high organic loads, presence of toxic compounds, and seasonal changes (Mueller *et al.* 1977). To counteract these effects, a biomass support material (Welander *et al.* 1997) or lagoons that are inoculated with commercial inoculum are introduced.



Performance of 1nxtures of Saccharomyces and non-Sac1arolnyces native yeasts during alcoholic fermentation of Agave duranguensis



Marrha Eugenia Nunez-Guerrero, Jesús Ilern, Irdo Páez-Len1 1a, Oiga Miriam Rutiaga-Quinones. Silvia Marina González 7.- Her re ra. Nicolás Osear Soto-Cruz

Departamento de Ingenierías Química y Bioquímica, Instituto Tecnológico de Durango, Felipe Pescador 1830 Ote, 34080 Durango, Dgo., Mexico

article n ro

Nndt!U'IIY Rr<n\,;:d aJun201s

kl'C(i\|d In r<!Yi:ed lot m M October 201s /v:ccpfd lij OC:lober 201S /Wallablcool,ne J.OCKmhct1O15



11w, 1il1t Ncohi::!14 (ete nl.tillQFI SCMt'I,I,n.tl i.\

abs11 act

Agave jmce is fermemN1.ind dsl1llt'd iwice m ord(r io ob1.1ln OlfI(.).I, .1tf dlltonol sp1nt bevrage.Tite go.1lof this .nudy wos tu select. yeast or }'C mtX(llr<'5 ,h.,>r co uld be ukd m mdultrial production of

lug!H,quality mc.l.cal Yc,uts 1sol.\t{'d dl1llOg fc:mlf.'111.J1on ul Agaw dura ucnsis wer<' tes-ted w ;denffy 1hc be-st urains wnh resp<c co1he <:hcm;c.11 ,;nd O1ganolep,ic ch.>r.t(t,msucs or tht ptouced mczc.11 l' hree 1n(l\11du.\l ye.ist lram were "it'!(cted lli' funhet swdy ro,ul.tsp<,rd ddbrut:ckillram rrrHI-00Ma, 5.1(.ch.uomyttScerl'Vi;iat' strolin r1m,OOtSS. and Klu 'Vcromycr:.marxianus <StnlN ITO OOM?. An,dysou uf 1hc response surf. 1c l>e1miucd identlñcahon of thre mocui.tnt\.; one mi,m,re(7S'.rS.cc1t"V1s1ac.nu OOJS5 ,ln:d .tsi L <klbruedal rT).OOfl,13'1 ;ind two j,ute SlidUb (100; K m.1rx.1anus ITO-OOM? ,ln<1 IOCYX S. t (f cvi -s1oéITD-00!8S ME>l.c.l1 m de, by ü ng lhc inoculam con.sirmed by 1\$%S.Ct'fevt.Ht: nu. 001 5 :md 251 T. dclbrUC'd:li rRO00014.1, (n, m;t:dmezcal 75Sc/2.STd) was ch t,,:51 in tel111! uJ y1cld. ndmess o! vol,aule cetmpnuorh. .jmi acceptabdtly 111 srnso,y t(>\$1S. Wt propo::'C' usmg this mixture OI yc-Jsts to dt'lielop .) prrxSuCI that c,m be used ;is "" inoculam In 1ndu tri.tl production of m{l'c.l1.,n (I 01ht""f, s 11lrt1S from dif1creni ave,"J){>Llt>\

2015 Elsevier Ltd. All rights reserved

Introdu11on

Fcm1t-nl.1t1on proce<'ds sponldncbu ly dnrng productJd11 of mci c:.11by artisan methods {). le IS dunn chts s1:i3c th.11 soluble-sug.1rs .1.1.e transformed imo elhanol anc-1 o t h er compounds. Th fin,t day) Of Jlccholic fermentation an_ .domlnat'edby mt n S.,crharomyceiyéel!.ts fromthegenera Candi.da. Kluyvc:romvces.lb ruJaspora, .and Pidua. .tmong others(1 1 1) _ 'hcese ye.JSts have low fetmenl,,ti'Ve capacty but generatt• various fl,wor compounds, 1nr11.1dmg cerpenolds, C:-).1trs. higher alcohol.s, glycerol. ace ta.ldehyd c.', accmc lCid. and succuuc .lcid(1). Af<cr Lhí'.sc fir.).1 d.aysof rermntatlon. non-S1ccharomyccsyéi:U)t., Jr<' re plJred by stt.ain:; of S:n:haromy<'6 ccrevistá, wlurh comp!N• R4111{-nt.m un (1 *, 1).SJ)(,nuneous fennént.iticm cluring anisat1 producllon of mc.ical h,ls two undes-ir.1hlc ch.Jr.lcrer1snsc: lh E'

fN ni en ta uon timecanva!)' from3 to 9 days, ,rnd the conc-ent ra üon

QÍ re-s1dual sug.cu h. v.lriabl'. A)larter cu11re (inoc\Jlant) can b< used to Mand.11thie the (ermeruanon process.mdloac.:lm:v(Ibetter 1111hz.luon of d)c ti:ro1c:nla bte i, ig:irs

In re-cent ycars, some stud1es h.lve uscd rnoncultures or co. cultures of S. t:f'f<'-'ViS!ác and non-S.1cchJron ces yeas1 Lo j>rodt.K!! MM(), mal\go win!(), and ol ugarc,,ne und pmeappte beverage (,). Non-S3cch.Iromycf.'S y aSt\$ conrribuco 1hc increased production of potysaC'Charides and can 1l)mh11ad the final concemlHI01s of a.e.11eac1d omd vol.l. -t1le-compouods (1). Morcovc1,11 hJs been sug- g<."sU. d1hat S.1cch.uol es and non-\$.lcch.,1rofTIY(esyeas ts mayacl synerg1sncdly (1} ror t-x.:unr,te, mixt>d culrures of cfocted ye,1.St'S h.1vc.- been developed as starter mocul,mt:; to l"nh<mce lhc (ucJllyuf win(1 11 11

), Selection of the .app1'opnate strJms is generally bil\$cd on cn1rri,1 such ,b fermenta!iv<' power. roJeraocc to cthanul. e,h,mØ y1('1d. toller phenoty)E", ;tnd low acetic acid i:>md u<tio n (1').

úwn \polti(li;ttJ.<Mh01' Erl\JI.address: " " (N.O.!M'itOCrut.



1 || PROVIN G Agave dI IrangI Iensis.MUST FOR E:!.I ANCEr> FER\,IEN TATI 0N. C/N RAT I O F:FFECTS ON \1EZCAL COMPOS IT IO N AND SEXSORY PROP ERT Ir:S

if E .JORA !VrJNT O OEL IMOST O DE A a,•e durmtfiuensis PARA LA FER JEN TACJO N ME .JOR AOA. EFEG: o s u j; LA RAZÓN C/N SOBRE LA COMJ OSTCLÚN DE MEZCAL Y LAS PROPIE DADES SENSO RI ALES

G.C. De lo Rio:-Dcras¹. O.M. Ruu:ig_a,Quhònc '.

J. l.ópc1-MIHnda. J.B. Púcl,.(cnnu¹,.vi t.6p(I.) N.O. Soto-Cnu 1•

1 Dc pa rumwm o dc lnj:emt'rrfJs Químu:a \ Bioqtllima,. h1s1i1uu, Tet'noMgteu ile Duron,,tJ. Jffr d, Ftllipc Pescador IS.J001,• C,,t Nta'l'tl \t: "'Yª. J4080. Oum nj:a l)ga ¹Un,dad1. Bi hfn ·nolngftJ r·Inxeni,•rftJ Geuhu·rJ ,fe /un, Ct'ntru dt'bm I lig" cüt ll \ E Imliur Ih" In:iiáus Jtd IJ'N. Ajmrrudt l' l'á i,(l/6:29. Inul maru. Gtu J65UO, /11'.•t.:ico.

Rccclv'-d ícbruay 22. 2015: ALq: rn; tJApriJ 27, U15

Al,strict

Mezc l'II j,,:tra dil u nll d, u llcdp fn b...;rage\bt.un,;J h · an ls.in ft1111..r". 11.10l\ •J:ig:nsug.ir: nI lhis....nr \e d termin d

dk dft.-cbuflh c:C/Nll l1:)) d lhc llllll...do 11c:dlmu iu n \f sugars mA'<,wt•dtm Inx Idh ;, m ul: u u lhc enue n l: l10ll li 111t ;,;. com j,.,óion anJ i.t<nsolytv .ll ilion of the mejc. I produc(d. 11k· re.11nt'mollfon ni A dur11ngm'd \l, llllll•ya enhanced hy aJd ing 'iC9r moreni hg -;n 1,c,.pi:ct l(l lhc nrigl111Icol11cr1U,b •11Hü •mum,11fate:el ,111milirII ;,ugar i.mcc m f .dllnn ol l"iJ g/L '11,em i.li.<0ll d lín m the mwa 1m:rc:ise;J lhc plódui:uon ufclh:mol ulil \Olauk •>hpou,d j; ,o.·h as eih}hct:llc,

2- hu i:im nldn-prop, u l)ll but dcc rc.;)SeJ lhc 11moulu(! JL'tc wid. dun ng lc,mcnt:nion llc : ,cct >áb(hh) ói lhc fina

pr odct was als,mc n;e d . Thœcm rnen:dl J.ppl.:;110111) f 1 hc inurnl t'0111 d i1b n, In lhc m11sl'rdmJ)O"llón :lll h np rove lhc f f lducm o f nK :t.:al. "óIH.i: Íl nm)' IJIt.:l'éa lhc: protict ieo..) of 1,1w m;lc ri:lh. Jcannng k-ih fC\$.ldua.l ugar JJIdm pr ó Vt' pmdu c:1.lcccv mhtlily

h l!h '()rd.r C"/N ratio. mczc.af t ompomion, vof:nile mctahohtc. . ens.ro y cvaltuumn

RI:sumen

1.1hczc, ll c.na bchi, il rh dk jm:iJ destilad: ql,u.:>c ob1knc por íermc.nl.i ión de:lo, a.t.üc.ars de :ff:J\c En cMdn b jò se dc(l mllaron 10>e-(cc10>de t 1rciaL:itín C/JN)' fa cõnceHrac10 n 1111d:!)dé ;,vite.ues.t:ld mostodf:igm " clum g œ.1fi:i o l>A fo ai C lii:a J.&rmcmac lón,l..iW lllf)<\$fi.:lón)' la t:\ lu1ul d1 11sç,j;Jdd ma ca) p'00œ Jo l ff ..ment ael <n del mo tu tic A d"rrmgut>,t i" fue m<Jm-ad.m dianle ll, 1Jicil n de un O",i di.! nllrc t-uo,l <4-pN k' ial c-m ten hln or, nal, C'Ont(\ >ul fjo ., de ill11on10:• un <0c n t mc dn nuci:d de 11.1.1kar de 150 8/l. l:.,uh CC1ndic,one,l nk il,é i; <n CJ nio:-10de ícnnctut<"ión

pcrmn, mn el umcto <leb rr Lx,111.:clun Jede et:mol compue., tm , ol,i lile . tille;comol ct Luu de e.ulo,2 hu l oo ly n propa nu,l a4-ic:ulll l,l<bnun uónde Ijje 11111d.-dde:k:ld>uc.tico,dural11 kl f;:,rnh·nú;iln l.ull rep ,:bllld ad dd prt.lducm tin:sl rinbi ln e 111cnmc n ló.La pt hcJ..iInl<omc rcial dé L'<a:.....omlicionc\$ Imu:..l,k en l't lll l t p'óic iú 11 ckl mc,-.10u <d..!

mc j .f.tr d pr fú é.\$0 dl" lñ duc c lóndi: m t.col, yn 'IU! pue,lt :ll ln"lCr.1;læ11,pmw,:h:nh l UI d')a;<mmtn1.l p runa de,:uxk'l menos uzúe-ar rcsl<tu..11)' mejorar lti acclp1.ibll'd:,JJd produ,:10

Pa/r1br,l du * <rc lacJn C/N, cr,mposit'lñn del mc,..c.it. rnc,abo hh>. \Ollules C \ilbi aq ón scn únaf

• f_m „ JJt•ndil1 ,u,1Ji<ir t:.mm1 : rso t.ollitd1U'3."igo.t"dl.l :u ITT1. '\$6/X >IJ-N ó:J.U., l'tl Jij'J, f <.t* 1... ,I f,1'1'1 xf);J \, 'J•

Full Length Research Paper

Characterization of fructans from *Agave durangensis*

Alma D. Orozco-Cortés¹, Gerardo Alvarez-Manilla², Gerardo Gutiérrez-Sánchez², Oiga M. Rutiaga-Quiñones¹, Javier López-Miranda¹ and Nicolás O. Soto-Cruz¹

¹ Department of Chemical and Biochemical Engineering, Instituto Tecnológico de Durango, Blvd. Felipe Pescador 1830, Ote. 3-080, Durango, Dgo, Mexico.

² Complex Carbohydrate Research Center, University of Georgia, Athens, GA 30602, United States.

Received 23 January 2013; Accepted 12 August 2015

Agave plants are members of the *Agavaceae* family and utilize crassulacean acid metabolism (CAM) for CO₂ fixation. Fructans are the main photosynthetic products produced by *Agave* plants, and are the principal source of storage carbohydrates. The aim of this work was to determine the chemical and molecular characterization of fructans from *Agave durangensis*. Fructans were extracted from 10 year old *A. durangensis* plants. Trimethylsilyl derivatization was employed to determine the monomer composition. The linkage types in these carbohydrates were determined by methylation followed by reduction and O-acetylation, and finally analysis by gas chromatography-mass spectrometry (GC-MS). Samples were shown to contain 1,4-D-Fructofuranose, 1,4-D-Glucopyranose, 1,6-D-Glucopyranose and 1,6-D-Fructofuranose linkages. The analysis of the degree of polymerization (DP) was confirmed by MALDI-TOF-MS showing a wide DP ranging from 2 to 29 units. The analyses performed revealed that fructans from *A. durangensis* are formed of 97.11% fructose and 2.89% glucose, and are a complex mixture of fructooligosaccharides of the neo-fructan type containing principally 1,3(2-1) and 1,6(2-6) linkages, with branch moieties.

Key words: Degree of polymerization (DP), GC-MS, MALDI-TOF-MS,

INTRODUCTION

Mexico has been considered the center of origin and biodiversity of the *Agave* genus, due to the taxonomic diversity found within its borders. Of the 310 species reported, about 272 can be found in this country,

Members of the *Agavaceae* family are distributed throughout Mexico, and are well adapted to both arid and semi-arid regions (García-Mendoza and Galván, 1995). They have undergone both morphological and

Corresponding author: E-mail: nsoto@tdurango.edu.mx. Tel: (+52) 618-8186936. Fax: (+52) 618-818483.

Abbreviations: OMSO: Dimethyl sulfoxide; TFA, trifluoroacetic acid; EtOH, ethanol; HMO: hexamethyldisilazane; NaOH, sodium hydroxide; CH₃I, iodomethane; NaBD₄, sodium borodeuteride; NH₄OH, ammonium hydroxide; NO₂, nitrogen dioxide; H₂O, water; CAM, crassulacean acid metabolism; PAAMs, partially methylated alditol acetates; WSC, water soluble carbohydrates; DP, degree of polymerization; GC-MS, gas chromatography-mass spectrometry; MALDI-TOF-MS, matrix assisted laser desorption time-of-flight mass spectrometry

hlcntification of a ycust strain as n potencial stuck whu. fermcnh,tion rtsnrtrc: a kinetic charactriz.ation

Idcnli ficali cln de u,rn cej,a de lc,ad ura con potencial de reinicnr fermentaciones , nicas es lunc.ndns; una caracterizaci3n cin3lica

L.Rodrigue,-Sifocntcs .J.D.Pic.r-Lcrna 'O.'.i. Ru1 la,ga•Qulili'ln(•\ J.A Ro las.(Cl)n1rer:is , F Ru11.-Baca . (i Gul1Crrc1 S:inchc,,; í. Banioi ttnd " Soto-Crut"

"Dt>p,Ir111mt11to u l n,c;en1<,n, . Q,mnlo.l l. Rluq11fmf'(l, Jm, 111,,J 1:r11ülvg,, u ,lt• D1rmgo. 3dfJ, fJ o, r"mJl•tl• '1f,•ltr,•o, "Fl,c:hold de Cle11tfru Q11fmir.u, Uul\:-t-rsrrlml Ju,irr, .lcll: t111lu., D1m111eu. J:()JQ D11ru111,u, \lt; ;wv. 'Complr!Y C:Jrbolr dr, lt r U uan.h Ct!lfi>r U,m1'r,ily uf r:r()7Tij Jnfio} Athc 11s l, ,j ,fD•pt1rtam,m1r1 J.-Gt:m:tk«, Umlvnuut ,11• Vu/Jucfo. 4MOQ Rur/,1.,-1"1, Spm)I !Rc<.mic:d i) Di:rcmr:r N1J: _rwuf 'c'v()w r't'nmed 5 hd,rimry :tUJ)

Re\•r;er)C3tt.Wun.: ;lw Ir9.XI h.l..oru.urnc r,ldul1I asui;l1r ln1:11nly lni, -) 11,q1..d.: wuw \•rm.n1111; ,m,1u 11 i-#l "tL '>1u,l,1M 1\... .. ll: l'e l,111•lt lly S 11u" 111). Y110 !l ;J10...:l:l:h •h1 h,1,l...h.1...t,•t th••mn),lnt.1'l it1\lotb ru-c, d \ m w 11111.4... ;,, o.1111,1,m1pio-1, .t1: ,11..TJ nu unwn cUil1MI pr,tJU.U<ln r,l: 11)14), O 26:-: • r.A.O.Z;1" 1 t.:>?"' \:h) •lli,ftf'foJro.,11 1\,s i.:l: -icd !O!fol 11 "t)l... :yb t Jtld lu:t'11c 11..dl.l) . S ltn.r ;inalu; i<J..ntifkd lb:- iw Jlit- lb .•i.u-cJr.irr; ,m,c,"J.1- (:.'1'111.;r !-tr,1 ill m)-00(1bl1, l'.t'OSl.ild 1 00 % ;:;vJ)(•"" ;:(1t1,• í HIOl:;<Jit r!'li 't.11 (ti 201' Alfil JV"t'.t.:ipe"t:U:t:Jyt whto cu!1L:dlñ inced..wn widl 12 .lv\•t chJiOOl '11é iruc1Qtlc (<füWllf!ti<ln Nk v. i,tc J; b) - q 7• " 11t3td" C "111:n cth.lmrol "h 11111i.tly plie,c 11 n t'w-mnlu. S, ,v,lfom•'l' Ú UIO>llw.i.<i<lo\;:,11,;ud, fi:'tld-"tliutm-11;111fi 1111;-and •,l;w. ablc!t\11111.1 ; tu 11m:n b h 11) n 114 h 1., a \Umn1Ct\i11111J\011.t.d.:m11.111 11'li haJ.) H'1'°1J1m• J1O,tJOD6ld\ a p.:t<ll.U11'Wll 11h 11 1 k 1111 j1 n,siarter- in \inc imj.d. fermcn.,:n,vn nl z'>•C

Keywords: fructose consumption; alcoholic fermentation of agave; mezcal

l;l,o;pt6 J, :ku1 di= 11:111C1.l&ftt Lhh;:,np,..111COht.rur k, \lfie.,r... n:<r.h1a! n"nJ)ollm'91t.:fl\1(f•J.;!;., ícrrn.:T\11, lunJe\m,r,t c<t1ln,l(1á;l :l: ,l.,Q 14:l e jMJt m'iu • nmu J4• lj ...j u, J: ICVd\Um J.a.:ern ITl).<l:l'INm1 n.1111 \:t'11r-s lta,I alm,;: del l' u,;ju n11i\lln1.; di: ,nx-nn.cr.!<•• .-on 1.JtTIO &- fü1.:1t1.:a)' rr(ldu.c. : fln ik c-1.l 1111 •0.113. ú.2(Jo, a d 0.231 li '. l':(l\.:t1vnn/cnk). J'vr,111 t noi,... fü , ,ekccu'lr: iln r,ir:1 I,!\.f"• b, li,'r. nmili is nofocll-r;1) c1001cM l.M v1'v ,il<:\(lon:11.h la <<pi! JU\• h.i.n11•l-nrla pl'r m.ti111 Rfl ' f ' I)lllv, S.:;rlum11t11\'. (U\1v1ia.- l.:i<4;:i N0 -0111);j C:1)\$.11,0)\1ÜI>"r } , • tk J tit.l:c)\t pr,•i.T'h'(11 1)"(:... l' l, h.1.J.N'aiv3tl1cct 1<wtdllk) "" cu)uvóé1y W enc,ho (•1U una oocIC'ifrn...: "iutml<1111,k IZ" (\•.) J: .!lam11 bl 1,,a.c.l.\:O1h1.1,k fruct1.1 ,je 1v"Ü)Q (11\11')7%a 10" T •l.lm,lo..j w11>X.;sh110'pw l'11lt:c.lc.J.:! uno;:,u.; m.:d10d\•u 11b\l'.) t l'R" \i1 , • fT1).{lij(tfll(:i:n ,1,101,<tlllthi-iunc. <fo ilm "ñh. 1111 . lám::;cl,a Vfú.;C.l11/ J: cl.lmplr<11rt. <cmx:n!-li;:,nen I M h 1-n tr ,11,, 111,i.,.,.,j11,-in\k '1U:J... """"tmljU.:; , ,,,\;tan N ITO-(k)()(:;u 11'ca11,hd11,1 p0cct:"ial pum s/ 1H1.<<Jtl'u,, , r1.'111C11d11 -et!u.f:ffik'l(lb!V1\ ,1,m.;ii:11, :!()°C

r-111.bfsad :1•f-l: cnu uu (Id.:fnR t•.:a, (cr.nc1,t.:t-111i J.l:c<•h&h,.. Je a a.,• 1-r. r.;;J

J111r od uction

Wmç j uJ uct.ñn ls.i --omp c prnc ;:, wh.:re yeas.:;j (pn n(1 11 {j((, 't'p r.rn1'c .l.c. , , , ,;iael m:nsform .sugars prc.;; u in grnpe ut tc;: mto 1N11u,I, C'O, .ind clh.:r 1111pon:ml n\11.100 htcs a;0 . :.rn1.;d w 1h Of:in,1kph1: qual111 " (l'crel. •C01.'11,,. iln ol1c.,;Pi=,1/, Ubl..dt1 hl.ltv.o , & M n in-Al,mcz, l'1' J) Onc ol hi: mo:-1cum

morproblcms q.) f1C1J11" d ,.,ith w1J\1! produ.:tion > l.rck Fl!nni.-1.,

1:11i1>n lhu resuhs whl•n wa.1-t>:ll,pr rn.1.th<tu: ac1J 11cis and "uiani prcu,il11.,r.lpc 1u1.;1; m: oot .:ompl.:tt;ly femu. •lu1.,J(B1s1td,n 1+;< i) lintr.:ldMfüx:dsu1vUw- re uh in lowc, clb.mol yidJ.: am! conta1110:ñu uf the tin.d plodu.:1 wuh n.,1; \e1mcro,11.;m1sm.: In:iddi lion, i .swtt<il;wor 1s undesirabc endry wm s IBm hcJi; (rnJcm-Oicr,\, 8.1U<.r, r'hc.,•1 m. & Prcw'l'üJ -11.)

Sevc 1:il factors ul<:Jud1.ng nulnen1 cl fiCñete .o. 1nd 1he presaneeof 10.xlc oomp) 1nd lhwcl:l(11 ik mdicd .n>auS(-.:; IC';<ftn In \u.:kfcnn nulionolndn1..1rac-1.syncbrnoulymye<1s1cclls (r\ k"1.fndrc- & Ch:irpenucr, 1 ,.: Uis" Mm, •,•,• J)on b k &

h11.:f11m. ln>]!"aCU & Auultc. ,.,,1; M:uocfo. (iu1J), & Or1.:;g), 1'1, r,unputtrn & f,0ur,;1ro•D'.u.s., "•O; Salmo,n 1 •) l:1hanol h\h:Cly 1s un.; of ch.: most tt1f)<m.lm 1 .:aus,,:; tr) 11m prohrom ("l.: "and."C & (' h:itp;OlC'r, 1'19;:,; H.kson 11, "1 1As to:m)h 1:l1io n pr., -c(!;:,cdianol cc,n.:cnm1 uns m(r lsc :11'h1 me ye.fj.,. llrams rr.ay b.: lmubl t>1simw under tbesc 1.,mJ1(.vns 117

1h ss mc lím.: t:ltunol r u11, iu dcc-rea.-!-cd sug:ar consumpton

f; f1S1J1.u.y(;<ak-o1c.Ulomhn. OI-tjUill. & Sabla)•r111c:1. _c11111 t Ounog mnc r.:nn r.l.i.l ton, WUh! yea.:;1s oo-ferm,1•1(gl u o1:1 /ic :mJ fru.:tu : l:tvq;:,r; pn.:stnl 1n g16'pc JUi cl Yc.í;L- tL\p11) ' ,rdt.'1 t;hu,;:-1. • 1nst1:ad of f:uctosc í8 rnJ1ds . Corde ro-Otel>. Uaucr. T...h,nu,;., & The-w. ll'w-, """: fü:1bclsc1 al., _:11,4; f nmchvm. Clamcro. Amlyo-Loj,.:t.Oarno.,1;:; Qucrut, _IM'•I,anJ 11ccumu- 1.1tingfn.n:ti:>c<l)fü" 11tm11.m.,ti:>Ullm the development u!stuek fl.'nncnl.don •flí ,;j>n ,i.: Oul'<-c- '111) h ii,;. .kno,qj 1ba1 m n•n•1•1.n11e glucn.,é .md fructose .11-.: lrurt.!>1)On d 11m) 1heccll hv 1hc x\h r r t'clb (Rt'ltc-nh.1'lg< Fre tdc-1, & Ciri;ity. I- """:;

*Corresponding author. Email: osoto@induranga.edu.mx

Microorganism Degradation Efficiency in BOD Analysis Formulating a Specific Microbial Consortium in a Pulp and Paper Mill Effluent

Luis A. Ordaz-Díaz,^{1,3} Juan A. Rojas-Comeras,¹ Oiga Rutiaga-Quifión,¹ Si Marrha R. Morcno-Juncos,² Felipe Alalí,¹ Mondr Jgón,¹ and Sergio Yalc-Cervantes

Pulp and paper mills are a major source of pollution, generating huge amounts of intensely colored effluent that goes to the receiving end of a wastewater treatment plant. The biochemical oxygen demand test (BOD) relies heavily on the microorganism metabolic capability added to the seed material. The seeding material in the testing is obtained from sewage sampling or from commercial sources. Specific organic pollutants that are present in paper and pulp mill effluent can only be degraded by specific microbes. Therefore, common sewage or synthetic seed may lead to erroneous BOD results. In this study, specific microbial species were selected to evaluate their degradation efficiency both individually and in combination. The microorganisms selected in the formulated seed exhibit BODs in a reproducible and synergistic manner. The formulation of this specific microbial consortium can be used to develop bioremediation strategies.

Keywords: Paper and pulp; BODs; COD; Degradation; Formulation

Introduction: Pulp and paper industry contributes heavily to water pollution. The high COD (chemical oxygen demand), color, and BOD of the effluent (Sanghvi et al. 2008) is the main source of pollution. Biological treatment can be used as an appropriate quality parameter indicating the amount of biodegradable organic materials in terms of oxygen consumption (Pepper et al. 1996).

Most of the industrial effluents have the necessary microorganisms to realize the BOD test without adding a microbial seed to increase its efficiency. The microorganism to degrade the organic matter is measured by the BOD, and changes in time and concentration. Using microorganisms obtained directly from the process via isolation and acclimation improves the treatment (Kumar et al. 2010).

INTRODUCTION

The pulp and paper industry contributes heavily to water pollution. The high COD (chemical oxygen demand), color, and BOD of the effluent (Sanghvi et al. 2008) is the main source of pollution. Biological treatment can be used as an appropriate quality parameter indicating the amount of biodegradable organic materials in terms of oxygen consumption (Pepper et al. 1996).

Most of the industrial effluents have the necessary microorganisms to realize the BOD test without adding a microbial seed to increase its efficiency. The microorganism to degrade the organic matter is measured by the BOD, and changes in time and concentration. Using microorganisms obtained directly from the process via isolation and acclimation improves the treatment (Kumar et al. 2010).

Trabuaid-Udaytonn (2005) reported that the role of fungus was isolated from soil samples collected by continuous pulp and paper mill effluent irrigation and identified as *Trichoderma reesei*. It was capable of 79% COD reduction. De Oliver-Je, et al. (2009) evaluated the ability of *Bacillus subtilis*, *Candida guilliermondii* to produce alkaline proteases

y liw;u lm ica l s l luto Tecnológico ele IJur:rnijj0, lil,-d Fd11:>e Pesc«dor 18300t«, 3 40 80,
Dur a ngo, Dgo.j e:tJco: E-mj-ijj)· nsotr,@itduunis:w.edu mx

Evaluation of *Eichhornia crassipes* as an Alternative Raw Material for Reducing Sugars Production

Héctor A. Filato-Pérez,¹ José G. Rutiaga-Quiñones,² Cristóbal A. Aguilar-González,³ Jesús D. Pácz,⁴ Javier López and Olim M. Rutia Quiñones¹

Water hyacinth was analyzed to determine its cellulose and lignin content, evaluating the conditions for the saccharification process with commercial microbial enzymes. Plant material, including leaves and stalks, was pretreated at several temperatures (100, 110, and 120 °C) with different sulfuric acid concentrations (0.5, 1.0, 1.5, 2.0, 2.5, and 3%) and residence times (0, 15, 30, 45, 60, 90, and 120 min). Total reducing sugars were measured by the dinitrosalicylic acid method. The optimum conditions that maximized the yield of reducing sugars included a pretreatment with 2% (v/v) sulfuric acid at 110 °C for 90 min. The optimum conditions for enzymatic saccharification used the commercial enzyme Celluclast 50 °C for 24 h of hydrolysis. The maximum yield was 0.54 g of fermentable sugars per gram of biomass. Data demonstrated that *E. crassipes* is suitable as a raw material for products such as bioethanol; however, further fermentation studies are required.

Keywords: Bioethanol; Lignocellulose; Pretreatment; Reducing sugar; Water hyacinth

Cu111J<.fr,jürmct1io11 a. (lttwu:a/ and Hmt.htmt<ttl E11gmc L-r1JtL!/ Jq,urtmn II, Durango Ins1iwreof 1'tdmr,Jo:;,y (ITD), Blv,L i:,i;ile Pt>.V."1tfor J.tw Otf . Col. \1u:tu Vi:cayu, 34080. Durang>. D s_o. 1Wf:;,ico. Tel. (t;J8U999h}J r,1. (J/t>, h. Sduml of 1 uj:i11c, 'tlll. m J-ood n ,fuwl(H!,Yt'mwrsidcul Aficlmucm-1 de Sun Nlco/n's de Nu/11/go. dpartado Po\•111/SR},C.P 58)(I() ,!.,(on•h,1 ..tit:h. \h•-r.thJ, ,. Dt7mrtme111 ufFaml Scumn ulld Tedmology Sdwl o/ Chemisti") UmI-ersidwl. fr,tám,na de tv11/miln (}.fiteC . Blwl. t' C(Irrnn:n v José CánM11a;f.rln. Col. JtcpúMica. Srrlh/to. : .52,iO.<.:on/1111/a.,\léxico: "Correspo11d/1rg rmrhor 0111mi t1gl|C11tdl1ra 1tgo., -J1.11\

INTRODUCTION

Water hyacinth, a freshwater aquatic plant, is native to Brazil. It is an ornamental plant found in different countries around the world. *Eichhornia crassipes* is used in traditional medicine and to remove heavy metals from water bodies (Ganguly *et al.* 2012).

E. crassipes is considered a weed and sometimes even a plague around the world; however, it can potentially be a resource due to its high carbohydrate content (18% cellulose, 50% hemicellulose). *E. crassipes* may be an excellent source of sugars, which can be fermented to produce ethanol. The bioethanol production is achieved through three steps: pretreatment to liberate cellulose and hemicellulose; hydrolysis of both cellulose and hemicellulose to obtain free sugars, and then fermentation to convert the sugars to alcohol (Singh and Bishnoi 2013).

In Mexico, utilization of new lignocellulosic materials for biofuel production is of vital importance to the future of bioethanol. The use of lignocellulosic materials for ethanol production is favored by abundance and low cost. *E. crassipes* grows very fast under the climatic conditions present in some regions in Mexico (Kumar and Wyman 2009).

Effect of glucose concentration on the rate of fructose consumption in native strains isolated from the fermentation of *Agave duranguensis*

M. Díaz-Campillo · N. Urtiaga · Ó. Soto ·
E. Ferrero · J. Rullán · J. Pérez

Received: 9 January 2012 / Accepted: 3 July 2012 / Published online: 11 August 2012
© Springer Science+Business Media B.V. 2012

Abstract Studies on the effect of glucose concentration on the rate of fructose consumption in native strains isolated from the fermentation of *Agave duranguensis* were carried out. The effect of glucose concentration on the rate of fructose consumption was studied in 11 native strains isolated from the fermentation of *Agave duranguensis* in the presence of 100 g/L glucose. The results showed that the rate of fructose consumption was significantly higher in the presence of 100 g/L glucose than in the presence of 50 g/L glucose. The optimal glucose concentration for the maximum rate of fructose consumption was 100 g/L. The results also showed that the rate of fructose consumption was significantly higher in the presence of 100 g/L glucose than in the presence of 50 g/L glucose. The results also showed that the rate of fructose consumption was significantly higher in the presence of 100 g/L glucose than in the presence of 50 g/L glucose.

Keywords Fructose · Glucose · Fermentation · Rate

M. Díaz-Campillo · Ó. Soto · E. Ferrero · J. Rullán · J. Pérez
0123456789, Universidad de Burgos, Avda. de Burgos, 112, 47100 Burgos,
Spain
E-mail: mdcampillo@alumni.upb.es

N. Urtiaga

Departamento de Microbiología, Facultad de Ciencias Exactas y Naturales,
Universidad de Burgos, 47100 Burgos, Spain

Departamento de Microbiología, Facultad de Ciencias Exactas y Naturales,
Universidad de Burgos, 47100 Burgos, Spain

E. Ferrero

Instituto de Investigación en Recursos Cinegéticos, Departamento de Microbiología,
Universidad de Castilla-La Mancha, 45011 Ciudad Real, Spain
E-mail: ferrero@urc.uclm.es

Effect of glucose concentration on the rate of fructose consumption in native strains isolated from the fermentation of *Agave duranguensis*

Keywords Fructose · Glucose · Fermentation · Rate

Introduction

Glucose and fructose are simple sugars that are found in many foods. The fermentation of these sugars by yeast is a common process in the food industry. The rate of fructose consumption is affected by the concentration of glucose in the medium. The present study was carried out to determine the effect of glucose concentration on the rate of fructose consumption in native strains isolated from the fermentation of *Agave duranguensis*.

The results showed that the rate of fructose consumption was significantly higher in the presence of 100 g/L glucose than in the presence of 50 g/L glucose. The results also showed that the rate of fructose consumption was significantly higher in the presence of 100 g/L glucose than in the presence of 50 g/L glucose. The results also showed that the rate of fructose consumption was significantly higher in the presence of 100 g/L glucose than in the presence of 50 g/L glucose.

The results also showed that the rate of fructose consumption was significantly higher in the presence of 100 g/L glucose than in the presence of 50 g/L glucose.

The results also showed that the rate of fructose consumption was significantly higher in the presence of 100 g/L glucose than in the presence of 50 g/L glucose. The results also showed that the rate of fructose consumption was significantly higher in the presence of 100 g/L glucose than in the presence of 50 g/L glucose.

Diofa M Nuñez-Ramírez
Jose J. Valencia-Lope
Fau, to Caldera
A uiles Solls-S 010¹
Javier López-Miranda
Hiram Medrana-Roldán
Luis Medina-Torres

Vt Cóa e... Al m.-riros)
SIL'fr',.tlnO:J. fr-:-.:11:i,
Tec.,olt-El't'i><!.a- C.1u1Jr;
Di. rH\go.Mf' u.

**Departamento de Procesos y
T...**

A...iiO-tlúm1 I,-•ut>o ,•tn.,\
C óof:iri1. i; t,11?:\e.,; (J F
f,It.' o

Oepan.arn"t'll4.> ,fia-1.,t!j.11j e•
Qu1111,cj F;::1.,:..: d ,•,
0,1 nucd fd • E" t.;t.<11
Vr \t-s.....:1... M ,,, tr11
/.,;J:Ón.,-nt1 Cw \¿.1.1.:0 :)\.,:f.,j
\i-":; ,: 1 , rñ

Research Article

Mixing Analysis for a Fermentation Broth of the Fungus *Beauveria bassiana* under Different Hydrodynamic Conditions in a Bioreactor

Abstract. The present work aims to study the mixing characteristics of a fermentation broth of the fungus *Beauveria bassiana* under different hydrodynamic conditions in a stirred tank reactor. For this purpose, the rheological properties of the broth were determined, and the mixing time was measured under different conditions of rotation speed and impeller diameter. The results show that the mixing time decreases as the rotation speed increases and as the impeller diameter decreases. The mixing time also decreases as the viscosity of the broth decreases.

Keywords: Bioreactor, Filamentous fungus, Hydrodynamics, Numerical simulation, Rheology

Received: July 16, 2012
DOI: 10.1002/ceat.201200130

1 Introduction

The study of the mixing characteristics of a fermentation broth of the fungus *Beauveria bassiana* under different hydrodynamic conditions in a stirred tank reactor is of great importance for the optimization of the fermentation process. The mixing time is a key parameter in the design and operation of bioreactors, and its determination is essential for the selection of the most appropriate hydrodynamic conditions for the fermentation process. The present work aims to study the mixing characteristics of a fermentation broth of the fungus *Beauveria bassiana* under different hydrodynamic conditions in a stirred tank reactor. For this purpose, the rheological properties of the broth were determined, and the mixing time was measured under different conditions of rotation speed and impeller diameter. The results show that the mixing time decreases as the rotation speed increases and as the impeller diameter decreases. The mixing time also decreases as the viscosity of the broth decreases.

The results show that the mixing time decreases as the rotation speed increases and as the impeller diameter decreases. The mixing time also decreases as the viscosity of the broth decreases.

The present work aims to study the mixing characteristics of a fermentation broth of the fungus *Beauveria bassiana* under different hydrodynamic conditions in a stirred tank reactor. For this purpose, the rheological properties of the broth were determined, and the mixing time was measured under different conditions of rotation speed and impeller diameter. The results show that the mixing time decreases as the rotation speed increases and as the impeller diameter decreases. The mixing time also decreases as the viscosity of the broth decreases.

Full Length Research Paper

***Saccharomyces cerevisiae* strains with robust responses to fermentation stresses isolated from the alcoholic fermentation of *Agave duranguensis* musts**

J. Páez¹, E. Córdova¹, Ó. Soto¹, E. Barrión², C. Belloch³ and O. M. Rutiaga-Ouiñones¹.

¹ División de Estudios de Posgrado e Investigación, Instituto Tecnológico de Durango. Blvd. Felipe Pescador 1830 Ote., 34080, Durango, Dgo., México.

² Instituto Cavanilles de Biodiversidad y Biología Evolutiva. Universidad de Valencia. Edificio de Institutos. Parque Científico de Paterna, Apartado postal 22081. E-46071 Valencia, Spain.

³ Instituto de Agroquímica y Tecnología de Alimentos (IATAJ C.S.I.C. Apartado de Coireos 73. E-46100 Burjassot, Valencia, Spain.

Accepted 18 February 2011

Yeasts used in fermentation processes are subject to different stress conditions, including low pH, high initial substrate concentration, accumulation of toxic compounds (e.g. ethanol), and temperature fluctuations. The fermentation of mescal is conducted under variable environmental conditions throughout the year. One of the most important environmental factors is temperature, as autumn and winter fermentations occur at low temperatures, but fermentation temperatures are much higher in summertime. The aim of this work was to compare the response of *Saccharomyces cerevisiae* strains isolated from agave fermentations to different stress conditions and two different medium culture one mimicking metcal production, using agave must and other synthetic must development for analysis in wine industry. The strains isolated from agave were compared with a commercial strain used in wine elaboration, which exhibits good tolerance to the different stresses found in industrial fermentations. All strains grew in the presence of glucose and fructose irrespective of the sugar concentration, and low pH did not affect the formation of colonies. Differences in growth were observed among the strains at different temperature and high concentrations of ethanol. Only 28% of the tested strains exhibited good tolerance to high ethanol concentrations, a desirable trait for avoiding stuck fermentations. The strain ITD00185 was able to grow in alcoholic stress condition, consuming sugar and producing ethanol in agave must. This strain shows tolerance to the different stress conditions and may be a useful starter culture for agave fermentation, the potential of the native strains to be used to improve other industrial fermentation processes that involve low temperatures and high ethanol yields.

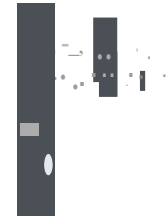
Key words: Ethanol tolerance, Mescal, native strains.

INTRODUCTION

The different conditions of fermentation processes can affect the growth of the microbes that contribute to the breakdown of sugars and production of alcohol. Different geographic regions and their particular environmental conditions can affect the distribution of native microbial

species (Folch et al., 2004). Microorganisms encounter many different stresses during industrial fermentation. Both traditional and industrial fermentation are complex processes due to the multitude of conditions that are created during fermentation. Yeast cells, which play a central role in the fermentation process of wine making, are never in a physiologically optimal environment during wine production. Throughout this process they are exposed to a variety of different stresses simultaneously (Bauer and Pretorius, 2000).

Corresponding author. E-mail: miram@itdodurango-bbquimica.com.mx



OPTIMIZACIÓN DEL PROCESO DE HIDRÓLISIS EN ZIMOLÍTICA DE UNA VARIETAD DE PAJAS DE FRIJOL DE (C. Arno) VARIETADES

(Pajitas de Frijol, Pajitas de Frijol, Pajitas de Frijol, Pajitas de Frijol, Pajitas de Frijol)

OPTIMIZATION OF ENZYME HYDROLYSIS PROCESS OF FOUR BEAN VARIETIES (C. Arno) VARIETIES

Optimization of Enzyme Hydrolysis Process of Four Bean Varieties (C. Arno) Varieties

En la actualidad, el uso de enzimas para la hidrólisis de almidón en la industria alimentaria es cada vez más común...

Recibido 22 de Noviembre 2010; Aceptado 8 de Febrero 2011

Resumen

El presente trabajo tiene como objetivo optimizar el proceso de hidrólisis enzimática de pajas de frijol de cuatro variedades...

Se utilizaron cuatro variedades de pajas de frijol: Pajitas de Frijol, Pajitas de Frijol, Pajitas de Frijol, Pajitas de Frijol...

Palabras clave: optimización, paja de frijol, hidrólisis enzimática, pretratamiento, celulosa

Abstract

The present work aims to optimize the enzymatic hydrolysis process of bean husks from four varieties...

Four varieties of bean husks were used: Pajitas de Frijol, Pajitas de Frijol, Pajitas de Frijol, Pajitas de Frijol...

Keywords: optimization, bean husk, enzymatic hydrolysis, pre-treatment, cellulose

Author for correspondence: E-mail: jlopez@itdurango.edu.mx

1. \ Jir 11¹, r¹ /i, j _lm, f 1211(i !/i 11). 1-!11 "HII
hur J,,1,, ion: 111 111.i;mh :11.,,qu: 1
lin,lp,uli: h.,J.,nlm:lul)..e.,e,l
pi"-f of" = 1.1' : \ 1-1., "IX- :



Study of the Rheological Properties of a Fermentation Broth of the Fungus *Be "laria hassi"lul* in a Bioreactor Under Oscillatory Hydrodynamic Conditions

1. \ ú fl- Ram írrz. Diola \ Jarinn¹. Lui, \ h-dina-Turr<. \ th i. Ja, it:r \ :tkl.:ia+.t',pt.l. F:11 lq (a l k n s:
. J:t\ierL .-JC' :li r in di JJiram .\k drano-llold:í n'. ancl ,\l uik, 0l ; , 111 11

;t mi uff,r 1, /, u, / /1HJ, Jtn,,Joi., Ti. (/111,,h.,,r a, í•lt/l., l, ll/f k, l, w i.: t, /, ,, , l' ,, , 1j/111 J, 311l > t, i Jr, , 11l > u, , mi.:o / > ., \A.U.,,

J: f: p, n \ p, n, 111 r d) < lrd1f11, 1, • /11., : 11, c-rm .l ; , 11/11 P/1 1/1 • m /, . \ < l P ll., Ju: , , , , 1, 11 l , n , l \ t " \ , \ 1, , , r - \ t V 111. / J \ , it 1 "
. 1, q • t 1" / tu IU 111 p, , , , , e. - \ ctu. l Tc. d JI(, f, g, ' , 1, / " " i l l . : • r 1 J i " " " i l / f i , \ t , l . l l H " (1 / J J I / h t f , t , , " - ') l j / \ t v i ,
l { \ , l . i 1 . : d \ p n l , 1 t .] O J t < , , 1 > . \ . J. J u h l 111 \ t r . p i : d u l h 1 . 1) i

F t 111: 111 l i o n " i t h l l , 1 t n l . 11 t u u , f u 1111 i n a b i o r e a c t o r l e t h b . l l
, t i m p l t . \ c J J n : 11 n k p r m : l . , t l r n t i s : l t t t . h e l h h ,

l'Ufl(lí b, u : m d l h e t \ o h u i o l l o f l h e r l u . u l o g k : t l n - u p < r l i l ' -
o r U u : n w d i u m . T h C : o t J r o p t • r r u s : t n • I n n i n l : i f f l " l . H e d H
h l • b i a m c o u c l n t n H i u n . i l l d l h r m o r p h o l o , u f l h t
r u u : : u s . I n l h i , , , o r l , , l h t • r h l ' o l u g i t . - : 11 p r o p t > t l ' (' : o l n
f e t r m . n t . t t i o l l , , i r h l h t . f u 11 l l , / J t . h l l l , r i " b t t , J w 111 u l u e r
d i f l ' c r e , l l H \ c f r n t h n a m i (- t . o n t l i l i o t b ' H . r j • l u d i t e d : i u l t h e t .
r h C ' O l o ; ! k a j h C ' l l : n i u r o f r h i h r o l h " a " ; 1 m 111 : H l ' d t h r n u ; ! h
t m h t u n : o f r : l r h o ,) m l . t h) l ' d l u J o w , u d i u m : m d ú • t u b l l .

fiber, (C \ (\ ' : l - ' F) . l h t . h i o n . a c t o r w ; u , a 1 0 1 (" I J H

: l m k 11 p e r a t , - c J . u d i l l \ - t ' u l , i i , c t u l r u • , t < l u - u h , l l C ' a l
l ' S ú s \ \ I T c . , i m l l : r : u 1110 ; U H I , l O O i p m l o r h u r h " \ ; , h 111 . J
l n \ \ t V < r . l t w r r H : 1 a s i 11 i f i c : t 11 f i n c r N l , t • i n r l i t . \ t , e i j : i l \
, , c . t m u , p r n i c d l l 11 c h r n i : t • i n 1 h r l ' O f ú ; i , h m t ' t . i n c t l • ,
t : d t : u l : t r t • d J I C ' r u r d i n t 1 (1 t h t : i o H e r J : t \ m o c d . f o r h t 11 h
; j , , h • i s : 11 S I I O I p n l . ' 111 l e . ,) , 1 t e n h \ \ h i h i r l ' d , h t • t h i o n i l i i .
l w h : i \ i o r : i r : i l l - t i . H • l o t i r i c , . \ \ h k h \ \ : 1 , l k t l . m i l l e d , , 1 h
i h l . D o w c r 1 : m m l k J d . ' J f u : m i \ i u c l l m c " • b u h , l ' t H . c l t o
i m n , j . 11 ; l h i : 1 C l l u l o s t • k , , n t l . u r i n r h , e . , , J N n i m n - i t d

a m i . l ' C J I \ \ (I I I I I H I \ , t h t . () O k i l . n t o f m i , i n d i m i n i J w t . l .
T b t l ' n o s u l h ! I I C r h u u g l u r u h e d u t . t u H u . r h l l l I I I ! k a l 111 d
m o r p b n l o i l ' a f i m i l ; 1 r i 1 , j . o l J I t • n , o t u n : 11 ' H h ' u l : , ,
T h e M r r s u l h " i l J h d p i n l h C ' 111 H i m i z : 11 i o n o f , 111 ' f . l l f)
p m d u t • r i u u o f t h < • s t • f u u ; ? i .

K t . , o n i s : R h . l h l g . , b y l l m J 1 l l m \ , ; ; r i l . m . m) , , , t w , j i t t ,
: - l m u l . l m 11 h 11 , j , w l . ' - . "

11 t t . l t . n m p f l a 1 h l l l b n • t h l • J 111 h T \ \ • f l . ! • t n l l l : - p i . \ : 1 . i l l

l h h : i u H I \ 1) 1 t d 1111 , , , , h i , 1111 , , o r l j) - n t h l . i , u , d p m x . l u ' !
1111 h : , n 111 i n u t m , 1 t 1111 . h J k . 11 u , u l f l h ' • r h < ; J o g i , : 11

p r n p \ . n : - \ , r t l l l ' : m \ . \ h u m l ' l ' \ l u l ' < - d 111 . d h i o l ' l . J 111 r ,
, l , r : 1 , , r . t i 11 , 1111 : l h u m i . ; l h : l i . r \ 1 4 . R ' 1 • l i : i 11 \ i n g 11 > t . l , t ' m
h • n n . u i - 111 11 k l r d . " d r l . u l a u , , u . l n J , : r l l u . , , : c c m d n i u n \ . 0111 : q j
l h \ . U h • , 1111 f u r J 11 t r r t , h h . n i . . . I P h \ . ; , l , h \ J t . , h 1 : t a t - h . . . h 11
t J J , U , f l t 1 " , 1 • m 11 . . e m < l p w \ . , : - d l g p a r . i m (" h : f o l o \ l i m ,
o u t 1111 • l u r 1111 h . n i t l h l l h 111 . \ 11 t 1 t h i . . r p r n h k n l . n : - - 1 . \ , \ h " u
m i . n . , t : , 1111 : - J h : - u d 1 . . . J i l . 11 n . : 11 h , u , i t U q . t r o d w . c t 1 1111 h L "

f . n 11 " 11 t J I h • l l ; t r ' 1 ; , , H I \ 1 . , l o l n - i : h h a r : - . l r , : - , í 5 J f l r : :

l h r t . u l - 11 - . h e ' 111 \ • I l h - . , t f 111 ; I 1 . 1 \ : t t i . , , l r l l i r 1111 , i o l l , I
11 \ . T \ 111 J . - : , : - , - k " I " , h 11 p r o < l u t , : h 1 p h l ' j . \ X P U . , . u u J I H U -
, , , \ h • 11 l i . 11 k m w l , 1 t t l u , n o u p , \ h - . n . : I H , l ' t , t r . : m , f i r u m . i
111 • 11 h l - : 111 , l r 1 h , n . l r . , , r " t r a 111 , ; < l . T l t i : 1111 p k u l i . m ; 1111 n 111
111 t t , t u \ . \ f l n l h . ! ! J o . l \ t 111 111 t i H 11 p l , l d t h 1 \ \ . : f i . • I H U I
l h . . . : - : P h • l k n l e 11 \ \ (\ \ 1 , r . l i w l ! 1 E \ " d l J n 1 E , l f ' t d n . " - : , l . : 111 , r " t h
111 c d l 11 . 11 l 1111 ; l k J J l r n : h ' h l l h . ! i l , • l l d 111 - n t n l . l i 111
t , . 1 - 1 111 r \ v . : 111 ' . ; , u . t h ; n . : h . l . , h e . - 11 l h n 1111 " \ : b H ! : !
111 . : r i : : 111 j h : ' ! ! (t i) , , 1 l l u : o p 11111 l i . . . , t i o l l o l l h . : 1 \ \ R

J I O C \ . - . \ \ d J : 1111111 , l d t t r n t . . 1 • 1 n h i 11 , g 1111 e . : ! 5 . . 14 1 \$.
11 ' j . l ' • t , r ú m h 1111 p 11011 1 - n r h , 11 f v d , i t : d l - x h J V a l 1 . (1 J ,
. m J \ " H . 1111 . . . i l . i r t l l 1111 q , l h • h • ! ! l l , 11 . m . t l . : , . f . 2 . • , 1 . 5 . (> 11
l i t 1 . 11 t h 1 . 11 i , 111 < l . \ \ \ l t h o m p k , 1111 . , r p h c i l ' ! : !) (• f t h i . . f ü n . ; ; i
111 \ P h . . . d . i l i : . d t \ U l i J l n 0 111 < l n n 1 , t i . . r l . : q u l r n 1 J l t f 1 . m l . l . r ,
. 111 J 111 d t h \ l p l t k , d . , h \ \ 11 f u t 1 r n 1 v i t h . : l l o , , p n • p . : r t i . . : -
: . n d 1111 . : ! ! ' u 1 J " ; . , , 1 l h i . h t \ t h t t , 1 p n • p i . : e , a l p 1 t i l ' w
11 , 11 t l , 11 h • l i : - , o l t l l h n l f l . m l . l . 111 , d U • J 1 p 1 Y : : , , , , , T h i . \ l p t m i . J 1 h

, , h , 1 : , \ 1 h . . . 1 : - J J : t l i . = a , r . l l , : t h , : t j x : j t l ' l i . m _ h _ . l . P 1
d i J I : : 11 j ' i 1 r t l t l l . l . e l \ \ 111 ' t l , L 111 : r 111 , : Lu i J . d J ; l l , H . , , h i c h
t 1111 r l . . . , , i r i J 111 111 , 1 . 1 , : : h , T h t 11 t , h . c h • u n j ; : . 1 • l

lih111i..nl1,u:.,hm!J,1-.1,;\rupk, rh1.11h) 'l'.il "'t.:111\ ,hT-'

\,lr 11,'...! , ,ilh tite,'-' Im cr1 lluj I :-,, t,m ... i... .. llr i; ;J... ,1

•e,1,,',,, ,..ll/h t.

, lnt, 11:1 11h1th 111..., · \.l.·" :"- ' u, 'b . liuw <10:-.1rmUI:-, ai u.J ..lbo

$uw/i, \mu$
fuuu' .1! .) ti! :; :; h1,eq.
f lu.1d.1h,·.f,lm-,r,nJ11h, lm.11 11111

ti:\. 1.1 1 ll,lt th\'. hi!llJ.l l,,, n;: flrJ11,bl ami llloq, lh ,J,,g |' |
lfü. ,., · l·r11h;,, 1.\lntriP1.1d.'-.lg11ilit"<mtl h·11mJ ilicJ #0 1b | thL.

rlz.: "" :h. ll b:h.i, " ,f 1,1! 11! .1.· q hll">. hi h \1,1,>,Jl .,nd

Full Length Research Paper

Effect of fermentation temperature on chemical composition of mescals made from *Agave duranguensis* juice with different native yeast genera

Martell Nevárez¹, Maria Angelica¹, Córdova Gurrola¹, Erica Estheta¹, López Miranda¹, Javier¹, Soto Cruz², Nicolás Oscar¹, López Pérez², Mercedes Guadalupe², Rutiaga Quiñones¹ and Oiga Miriam¹.

¹Instituto Tecnológico de Durango, Departamento de Química y Bioquímica, Boulevard Felipe Pescador 1830 Ote. Nueva Vizcaya, C.P. 34080, Durango, Dgo, Mexico.
²Centro de Investigación y Estudios Avanzados de IPN, Unidad Irapuato, G10., 9.6 km North By pass. Irapuato and Leon Carr, CP 36821, Mexico.

Accepted August 11, 2011

In this study the fermentation behavior at 18 and 28°C of different native yeast genera on juice from *Agave duranguensis* was evaluated and the volatile compounds produced in the obtained mescals from these fermentations were identified. The fermentative capacity of *Hanseniaspora uvarum*, *Kluyveromyces marxianus* and *Saccharomyces cerevisiae* increased at 28°C; however, the fermentation behavior of *Torulaspora delbrueckii* was not affected by temperature. In the mescals produced by *H. uvarum*, *T. delbrueckii* and *S. cerevisiae* a greater number and abundance of compounds were identified at 18°C than at 28°C. Conversely *K. marxianus* showed a higher production of these compounds at 28°C. Some compounds identified in all mescals were *n*-methyl-1-propanol, 3-methyl-1-butanol, acetic acid, 1-(2-furanyl)-ethanone, furfural, α -terpineol, ethyl phenyl acetate and phenylethyl alcohol. For strains *H. uvarum*, *T. delbrueckii* and *S. cerevisiae*, the most abundant compound identified was 3-methyl-1-butanol at both temperatures. However, for *K. marxianus*, phenylethyl acetate was the most abundant. The non-*Saccharomyces* genera studied exhibited different behaviors to those reported for wine fermentation when the same genera was used. Therefore, they presented a major fermentative capacity and also volatile compounds characteristic of mescals were produced.

Key words: Non-*Saccharomyces*, temperature, volatile compounds, SPME-GCMS

INTRODUCTION

Mescal is a traditional alcoholic beverage from Mexico that is made similarly to tequila. The process begins with

the harvest of *Agave* after 8 years of growth. At this stage, the plants are cut from their base, obtaining the *Agave* heart. Later, these are cooked in ovens or autoclaves. During this stage, polysaccharides, mainly fructans, are hydrolyzed by heat into simple molecules such as glucose, fructose and sucrose. The hydrolyzed sugars are extracted from the must by pressing and came out the alcoholic fermentation by native yeasts or selected strains. Finally, the must with ethanol concentration of approximately 3 to 6% (v/v) is distilled to obtain white mescal or young mescal with a concentration of 35

Corresponding author. E-mail: main@tposado.bioquimica.com.mx. Tel: 61829 99033 ext. (110)

Abbreviations: HPLC, High performance liquid chromatography; LSD, least significant difference; DVB/CAR/PDMS, divinylbenzene-carboxypolydimethylsiloxane; SPME, solid phase microextraction.